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Enhancement of mesophase formation in paraffinic-rich clarified oil using transition metal catalysts (Cr and Cu)

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Abstract

In the present work, we have made attempts to prepare petroleum pitches from paraffinic-rich clarified oil (CLO) by giving thermal treatment at 370 °C in the presence of Cu and Cr catalysts. The feed CLO is predominantly paraffinic in nature, so it takes fairly large thermal soaking time (21 h) to convert into pitch having mesophase content below countable limits. To increase the mesophase content in the pitch or to make mesophase pitch, 3 wt % transition metal catalysts (Cu and Cr) were added to CLO. Addition of transition metal catalysts not only enhances mesophase formation but also helps to reduce thermal treatment time by promoting polymerization and condensation reactions at a faster rate. The mesophase formation pattern reveals that Cu and Cr catalysts increase the mesophase content from below countable limit to 12 and 9 vol %, respectively. This indicates that Cu and Cr showed better catalytic activity for mesophase formation growth. The effect of transition metal catalysts on physico-chemical properties (softening point, coking value, toluene insolubles and quinoline insolubles) as well as the optical texture and physical properties of mesophase pitches were investigated by optical microscope, FT-IR, SEM, NMR, TG/DTG and XRD.

Keywords Clarified oil · Transition metals · Thermal treatment · Mesophase

Introduction

Mesophase pitches are prepared either by thermal [6, 13] or catalytic polymerization [18, 20, 22, 23] processes from low-value petroleum and coal by-products, i.e., decant oils. These pitches are complex mixtures of various types of organic molecules that mainly consist of polycyclic aromatic hydrocarbons (PAH). Furthermore, this mesophase pitch is very cheap and readily available, and has attracted extensive attention as promising materials for a variety of applications, such as needle coke [24], carbon fibers [36], Li-ion battery cathode [34], C–C composites [16], carbon foam [14], activated carbon [1], mesocarbon microbeads [35], etc.

In previous reported literature [4, 19, 21, 25, 28], many researchers prepared mesophase pitches from petroleum residues, coal tar pitches and pure aromatic compounds using

Lewis acid. AlCl₃ and HF/BF₃ are extensively used catalysts to prepare spinnable mesophase pitch from aromatic hydrocarbons. Among these, AlCl₃ was not completely recovered from resulting pitch, whereas HF/BF3 was easily recovered. Most of the previous works on catalyzing mesophase formation have focused on either minimizing the impact of the retained catalyst or on recovering the catalyst from the product. In our previous paper [9], we have used cobalt and nickel salts in petroleum residues (paraffinic clarified oil and aromatic heavy extract) to enhance the mesophase contents, pitch yields and other physico-chemical properties. Among these petroleum residue paraffinic clarified oil having very low bureau of mines correlation index (BMCI), i.e., 51 is produced a pitch contained mesophase contents below countable limit and pitch yield being quite low (11.88 wt %). Although, the presence of transition metal salts (Co and Ni) in paraffinic clarified oil enlarged the size of mesophase spheres, i.e., increased the mesophase contents, pitch yield and other physico-chemical properties. Here, the recovery of catalysts has done by refluxing higher-density part of pitch which was settled down bottom of the reactor with ethanol. As we know that mesophase pitches are used as a precursor material for premium-quality petroleum coke.



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This premium-quality petroleum coke is used for making graphite electrode for steel industries. Most of the premium-quality petroleum coke in India is imported from foreign countries for making graphite electrode and other carbon products. Keeping this in view, we are trying to explore different types of transition metal catalysts which enhance the mesophase formation in paraffinic clarified oil. This study will help petroleum refiners for production of mesophase pitch/premium-quality petroleum coke.

In the present work, we have made attempts to prepare petroleum pitches by the aid of Cr and Cu salts into paraffinic-rich clarified oil (CLO) obtained from fluidized catalytic cracking (FCC) process in petroleum refinery by giving thermal treatment at 370 °C. Pitches of different thermal soaking time are observed to examine the poly-condensation and mesophase transformation in the presence of different catalysts. Furthermore, synthesized mesophase pitches was also studied by applying several instrumental techniques such as FT-IR, NMR, XRD, TG/DTG, scanning electron microscopy (SEM) combined with energy dispersive X-ray spectroscopy (EDX), optical microscopic imaging, etc.

Experimental section

Raw materials

In this study, petroleum-derived clarified oil (CLO) from Indian petroleum refinery (Hindustan Petroleum Corporation Limited, Mumbai) was used as the precursor for mesophase pitches and its physico-chemical properties are reported in our previous paper [9]. CuCl₂·4H₂O (99%, Acros Organics) and anhydrous CrCl₃ (99%, Acros Organics) were chosen as the catalysts. AR grade toluene (99.5%, Loba Chemie), and

Table 1 Physico-chemical properties of pitches

Characteristics	CLO-0-0 [9]	CLO-Co-3 [9]	CLO-Ni-3 [9]	CLO-Cr-3	CLO-Cu-3
Thermal soaking time (h)	21.00	7.30	2.20	4.20	5.35
PYa (wt %)	11.88	16.22	15.08	17.42	18.16
MC ^b (vol %)	BCL^g	16	13	9	12
SP ^c (°C)	98	126	125	145	120
CV ^d (wt %)	48.97	56.69	55.44	57.30	54.96
TIe (wt %)	20.39	36.66	36.69	51.64	36.15
QIf (wt %)	1.08	5.00	4.93	26.35	5.51

^aPitch yield

gBelow countable limit



quinoline (97%, Merck Chemicals), were used as solvents for determining insolubility in mesophase pitches.

Preparation of mesophase pitches

A mixture of 170g clarified oil (CLO) and 3 wt % (all concentrations are expressed in weight percentage of total reaction mixture) catalysts (Cr and Cu salts) was agitated at 150 °C for 1 h and placed in a glass reactor. Thermal treatment of the mixtures was carried out with the help of heating mantle at temperature 370 °C under a nitrogen flow at atmospheric pressure at a heating rate of 5 °C/min. The nitrogen gas flow rate was about 150 ml/min for 170 g of feed using wet gas flow meter to provide enough turbulence in viscous pitch. The resultant mesophase pitches prepared from CLO were named as CLO-Cr-3 and CLO-Cu-3. In the pitch nomenclature, first value denotes feed stock, second denotes transition metal catalyst and third denotes wt % of catalyst. The physico-chemical properties of all synthesized mesophase pitches are given in Table 1. A schematic process for making mesophase pitches from clarified oil using transition metal salts (Cr and Cu) is represented in Fig. 1.

Characterization of mesophase pitches

Softening point, coking value, toluene insolubles and quinoline insolubles of mesophase pitches are determined by American Society for Testing Materials (ASTM) test procedures, i.e., ASTM D-3104, ASTM D-4530, ASTM D-4312 and ASTM D-2318, respectively.

Elemental analyses (carbon, hydrogen, nitrogen and sulphur contents) of the mesophase pitch samples were determined using Elemental Vario Micro Cube instrument.

The microstructures of mesophase pitches were studied with optical microscopy (OM) under polarized light

bMesophase contents

^cSoftening point

dCoking value

^eToluene insolubles

fQuinoline insolubles

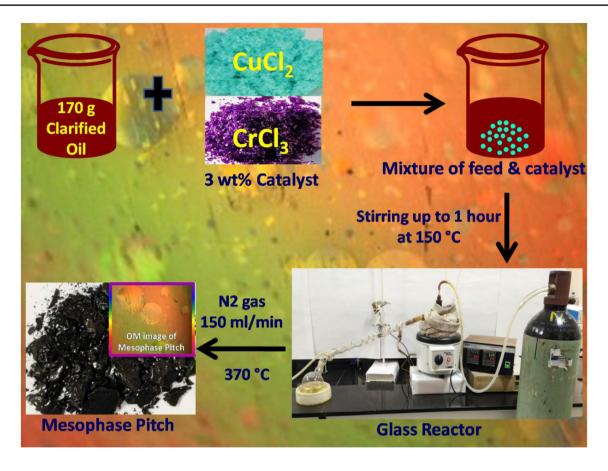


Fig. 1 Schematic diagram of experimental process for making mesophase pitch

(NIKON optical microscope). To determine mesophase contents (MC) in different mesophase pitch samples, ASTM D 4616-95 test procedure was used.

Mesophase pitches were analyzed by FT-IR, using a Perkin–Elmer spectrometer over the range of 4000–500 cm⁻¹. The KBr pellet technique was used in this analysis.

The mesophase pitch samples were characterized by liquid-state ¹H NMR and ¹³C NMR spectroscopy. The analyses of these samples were performed with a Bruker AV-III 500 NMR spectrometer with ¹H Larmor frequency of 500.1 MHz. For ¹H NMR and ¹³C NMR spectroscopic analyses, solutions of pitches were made in CDCl₃ and tetramethyl-silane (TMS) was used as an 'internal reference'. For ¹H NMR analysis, a solution of 10 wt % of the sample was prepared in CDCl₃; while for ¹³C NMR analysis, concentration of sample was increased to about to 40 wt %.

X-ray diffraction was performed on mesophase pitch samples D8 Advance Diffractometer, Bruker, Germany. The radiation used was the K α line from the Cu (λ =0.15418 nm). Powdered pitch samples were scanned from 2–80° in 2 θ range with 0.02° step size at a scan rate 1°/min. The diffractograms were used to calculate interlayer spacing (d_{002}) by Bragg's equation, $2d_{002}\sin\theta$ = λ [30] and

crystallite thickness ($L_{\rm c}$) by Scherrer formula, $L_{\rm c}=0.89\lambda$ / ($\beta_{002}\cos\theta_{002}$), where λ is 0.15406 nm, θ is the Bragg angle, and β is the full width at half maximum [15]. From d_{002} and $L_{\rm c}$ values, number of aromatic sheet in stacked cluster (N) is calculated by following formula, $N=L_{\rm c}/d_{002}+1$ and average number of carbon atom per lamellae (n) is calculated by following formula, $n=0.32N^2$ [15].

Scanning electron microscopy (SEM) was used to analyze surface morphologies of mesophase pitch samples obtained from CLO using 'field-emission scanning electron microscope—energy dispersive spectrometer system' (Model—Quanta 200 F). The surface coating of mesophase pitch samples were done with pure 'Gold' using EMITECH Gold Sputtering unit. The image of pitch samples was taken at 500× magnification using E.T.D. detector and 30-kV beam current for morphological study.

The thermal behavior and properties of mesophase pitches during pyrolysis were monitored by thermogravimetrical analysis. TG and DTG analyses were performed in a TA Instruments SDT 2960 thermal analyzer on 10 mg of sample placed in thermobalance. The temperature was increased from room temperature to 900 °C at a heating rate of 10 °C min⁻¹ under a nitrogen flow of 100 ml/min. From



the first derivative of the curves, weight loss with respect to time and temperatures of maximum rate of weight loss were determined.

Catalyst recovery: After completion of reaction, the entire pitch was separated into two parts, i.e., upper and lower, which establish the heterogeneity of the system. The high-density catalysts were settled down in the form of black-colored solid mass in the lower part of glass reactor. For catalyst recovery from black-colored solid mass, refluxing is used with ethanol at 50 °C. After refluxing, ethanol is separated from transition metal catalyst by distillation. However, in case of Cr, above refluxed method is not used because Cr is insoluble in ethanol. So, there is a problem for recovery of this catalyst.

Results and discussion

Analysis of mesophase pitch characteristics

In our previous reported paper [9], paraffinic clarified oil (CLO) took a very large thermal soaking time (21 h) to convert into petroleum pitch at 370 °C having mesophase content below countable limit. In our previous paper, Co and Ni salts are used to improve mesophase content and optical texture of mesophase in CLO. But in the present work, we have used other transition metal salts, i.e., Cr and Cu salts in CLO to improve the mesophase content and optical texture of mesophase. The prepared pitches at 370 °C were ground and characterized by following procedures described in experimental section. The main physico-chemical properties of these pitches are summarized in Table 1. Pitches, i.e., CLO-Cr-3 and CLO-Cu-3, prepared from CLO using Cr and Cu catalysts, respectively, exhibit increased value of physico-chemical properties, i.e., softening point (SP), pitch yield (PY), coking value (CV), mesophase content (MC), toluene insolubles (TI) and quinoline insolubles (QI) as compared to CLO-0-0 pitch whose properties are reported in our previous paper [9]. Cr and Cu catalysts used in CLO for pitch preparation reduces the thermal soaking time to 4.20 h and 5.35 h, respectively, as compared to base case CLO-0-0 (21 h) which is summarized in Table 1. Thermal soaking time is reduced because catalyst particles promote the polymerization and condensation reactions among the polycyclic aromatic molecules which lead to the gradual rise of SP, PY, CV, MC, TI and QI of the resultant mesophase products. These results were also consistent with the increase in C/H ratios mentioned in Table 2 which indicated that dehydrogenative condensation reactions take place during thermal treatment process. Therefore, the above results revealed that Cr and Cu salts are effective for the growth of mesophase formation.



Table 2 Elemental analysis of pitches

Sample	CLO-0-0 [9]	CLO-Cr-3	CLO-Cu-3
C (wt %)	90.60	92.04	89.10
H (wt %)	5.5	4.57	4.87
N (wt %)	0.09	0.08	0.09
S (wt %)	2.40	2.72	2.88
C/H	1.38	1.69	1.54

Elemental analysis of pitches prepared from paraffinic CLO is summarized in Table 2. This analysis showed that all pitches are mainly composed of carbon, hydrogen, sulphur and least amount of nitrogen. Elemental analysis of CLO-Cr-3 and CLO-Cu-3 pitch samples showed a decrease in their hydrogen content along with increase of C/H ratio (Table 2), which is 1.69 and 1.54, respectively, as compared to CLO-0-0 (1.38). Therefore, these results revealed that Cr and Cu salts promote the dehydrogenation-type reactions in pitches which results in increasing C/H ratio as compared to CLO-0-0 pitch. Furthermore, more value of C/H ratio indicates that polymerization and condensation reactions in mesophase pitches involved removal of hydrogen which results in the formation of highly aromatic molecules. Here, there is a possibility to some kind of interaction between Lewis acid catalysts, i.e., Cr and Cu and aromatic pitch molecule. The CrCl₃ and CuCl₂ also behave as weak Lewis acid. Thus, plausible mechanism involved in these interactions is similar to that of FeCl₃ [8], AlCl₃ [29] and HF/BF₃ [23, 25].

Optical microscopic analysis of pitches

Mesophase development during thermal treatment of paraffinic CLO using transition metal salts (Cr and Cu) at 370 °C is tailored by plane-polarized light optical microscope which is shown in Fig. 2. In our previous reported paper [9], pitch CLO-0-0 exhibits mesophase content below countable limit (BCL), i.e., no mesophase spheres appear after a very long thermal treatment time (21 h). The use of Cr salt in CLO formed CLO-Cr-3 pitch which developed 9 vol % of mesophase shown in Fig. 2. Optical microscopic image of CLO-Cr-3 exhibits large-size mesophase spheres along with tiny mesophase spheres which are heterogeneous in nature. Under the same experimental conditions, CLO-Cu-3 developed 12 vol % of mesophase which is shown in Fig. 2. CLO-Cu-3 also exhibits very large-sized mesophase spheres which are also heterogeneous in nature. There are no significant differences in mesophase formation among two pitches prepared using Cr and Cu salts. Both pitches exhibit large-sized good optical texture of mesophase spheres which are heterogeneous in nature as compared to that of CLO-0-0 pitch having mesophase contents below countable limit. The plausible reason is that CLO-0-0 contains less naphthenic

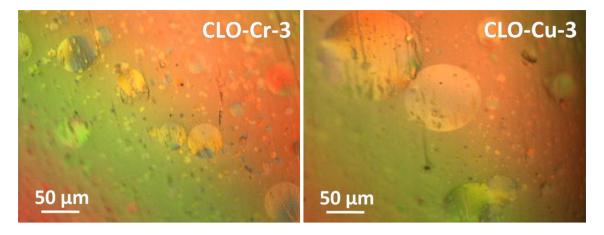


Fig. 2 Optical microscopic images of synthesized petroleum pitches

groups and more alkyl side chains, while CLO-Cr-3 and CLO-Cu-3 have more naphthenic groups and less alkyl side chains. Moreover, the alkyl side chains of CLO-Cr-3 and CLO-Cu-3 are shorter than that of CLO-0-0. The alkyl side chains of CLO-0-0 can be disintegrated rapidly to produce free radicals, which increase the polymerization reaction and also rapidly increase the viscosity of the whole system [5, 27]. As a result, the development and coalescence of mesophase spheres are restricted. Therefore, in CLO-0-0, mesophase spheres do not appear. However, CLO-Cr-3 and CLO-Cu-3 contain more naphthenic groups which lead to hydrogen transfer reaction during the pyrolysis process and maintain low viscosity of the pitch. Then, large amount of tiny mesophase spheres are coalesce with each other to form large-size optical texture of mesophase pitch. Therefore, the results presented above showed that Cr and Cu accelerate the mesophase formation growth in CLO due to faster polymerization and condensation reactions.

SEM and EDX analyses of mesophase pitches

The surface images of petroleum pitches are taken by SEM and are presented in Fig. 3. Figure 3 shows that both pitches have flake-like structure along with fractured surfaces. SEM images of CLO-Cr-3 and CLO-Cu-3 have more flakes as compared to CLO-0-0 pitch because Cr and Cu facilitate that various hydrocarbons are polymerized to different extent and at a faster rate. Generally, the fracture structure is formed when a large amount of volatiles is released which changes the sample into solid product by fast increase in the viscosity of the system. Reported literature also mentioned that mesophase pitches have flake-like structure along with fractured surfaces [2, 33]. The EDX analyses (Fig. 3) show that petroleum pitches are mainly composed of carbon, nitrogen, oxygen and sulphur elements. The aluminium and chlorine elements are present in trace amount which may be come

from mineral matter present in the petroleum feed stock. SEM and EDX analyses clearly show that catalyst particles are not attached to the surface of mesophase pitches which indicate that catalysts react with aromatic pitch molecules and promote the rate of chemical reactions but they do not mix with pitch molecules and settled down in the bottom of the reactor.

FT-IR analysis

FT-IR spectra of two different pitches prepared from CLO using transition metal salts (Cr and Cu) are presented in Fig. 4. Figure 4 clearly shows that both pitches exhibit approximately same intensity and same absorption bands at nearly about the same positions. The spectra of these pitches mainly exhibit absorption bands corresponding to aromatic and aliphatic structures. The aromatic absorption bands observed at 3050 cm⁻¹ due to aromatic C-H stretching, at 1600 cm^{-1} due to aromatic C=C stretching and at 870, 810 and 745 cm⁻¹ due to aromatic C-H out-of-plane bending vibrations [17, 26] which indicate the condensation degrees of polycyclic aromatic hydrocarbons. The aliphatic absorption bands observed at 2920 cm⁻¹ due to aliphatic C-H stretching and at 1440 cm⁻¹ due to methylene C-H in-plane bending vibrations [17, 26] indicate that a certain amount of aliphatic side chains are present in the mesophase pitch. FT-IR spectroscopy is also a useful technique to calculate aromaticity index of two different pitches by taking absorbance value at 3050 cm⁻¹ and 2920 cm⁻¹. The aromaticity index of pitches was calculated by following equation $I_{ar} = Abs_{3050}/(Abs_{3050} + Abs_{2920})$ [10, 12] which is presented in Fig. 4. The aromaticity index of CLO-Cr-3 and CLO-Cu-3 was evaluated to be 0.43 and 0.40, respectively. The above result is also correlated with mesophase content of the pitches. As the aromaticity index of the pitches increases, mesophase content (Table 1) of the pitches also increases



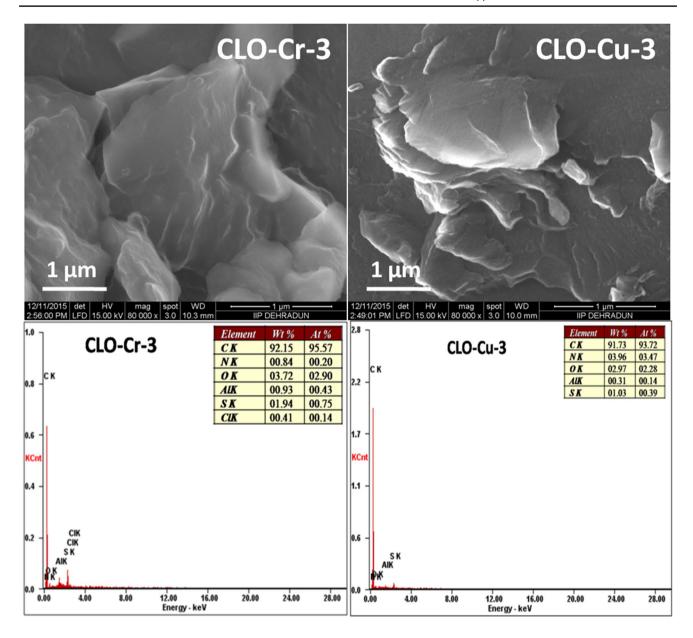


Fig. 3 SEM and EDX images of synthesize petroleum pitches

which result in the formation of large aromatic molecules by polymerization and condensation reactions. The results of the aromaticity index of pitches calculated by FT-IR are also consistent with the C/H ratios (aromaticity calculated by CHNS analysis which is mentioned in Table 2).

¹H NMR and ¹³C NMR analyses

¹H NMR and ¹³C NMR spectroscopy is the most useful technique for investigating the composition of petroleum-derived products, especially mesophase pitches. In this study, we have used this spectroscopy which brought the significant information about percentage distribution of

'aliphatic' and 'aromatic' protons and carbons, respectively, in both pitch samples. Integration regions used for 1 H NMR spectra were 0.5–4.5 ppm for aliphatic protons (H_{al}), 6–9 ppm for aromatic protons (H_{ar}); for 13 C NMR spectra 5–50 ppm for saturated carbon (C_{sat}), 100–160 ppm for aromatic carbons (C_{ar}) [11]. 1 H NMR spectral regions were subdivided according to the different types of hydrogen present in the pitch samples, as shown in Table 3. The normalized integration data of the different spectral regions of pitch samples are listed in Table 3 and their spectra are given in Fig. 5. 1 H NMR spectroscopy shows that CLO-Cr-3 and CLO-Cu-3 pitches have more aromatic hydrogen contents (H_{ar}) and lower aliphatic hydrogen contents (H_{al})



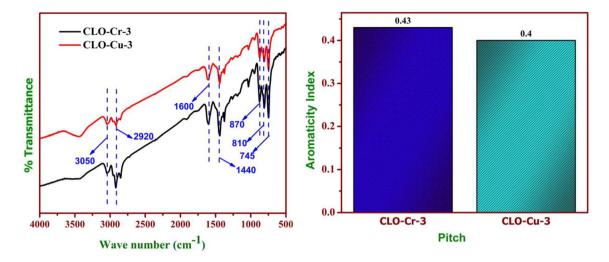


Fig. 4 FT-IR spectra and aromaticity index of synthesized petroleum pitches

Table 3 Normalized integration data based on the ¹H NMR and ¹³C NMR spectra of pitches

	Chemical shift range (ppm)	CLO-0-0 [9]	CLO-Cr-3	CLO-Cu-3
¹ H NMR				
H _{ar(mono)} (%)	6.0-7.1	5.20	5.96	5.26
$H_{ar(di)}$ (%)	7.1 - 8.2	42.86	70.86	49.17
$H_{ar(poly)}$ (%)	8.2-9.0	6.49	3.46	14.09
H _{ar} %	6.0-9.0	54.55	80.27	68.52
H_{α} %	2.1-4.5	26.87	10.63	27.16
H_{β} %	1.1-2.1	16.39	7.95	4.07
Η _γ %	0.5-1.1	2.19	1.14	0.25
H_{al} %	0.5-4.5	45.45	19.72	31.48
H_{ar}/H_{al}	-	1.20	4.07	2.18
¹³ C NMR				
C _{sat} %	5-50	11.57	8.29	9.90
C _{ar} %	100-160	88.43	91.71	90.10
C _{ar} /C _{sat}	_	7.64	11.06	9.10

as compared to CLO-0-0 pitch because Cr and Cu catalysts promote the greater extent of 'polymerization' and 'condensation' reactions which are responsible for formation of parallely stacked planar aromatics in mesophase pitches. Furthermore, the aromatic hydrogen (H_{ar}) contents of both the resultant pitches increase, and simultaneously aliphatic hydrogen (H_{al}) deceases, which also suggest that cracking or dehydrogenative aromatization process of the aliphatic side chains occurs during the thermal polymerization [7, 32]. In general, both pitches have more α proton (H_{α}) as compared to β protons (H_{β}) and γ protons (H_{γ}) which means that most of the alkyl groups linked to the aromatic rings are α -methylene which facilitates the cracking reactions

during the thermal soaking. These cracking reaction forms the benzylic-type free radical, which then polymerized to form parallely stacked planar aromatic bridge structures. Furthermore, if the pitches contained large amount of long alkyl side chains and alkyl substituents, then it would generate more free radicals, which make the polymerization and condensation reaction very fast and restrict the growth of mesophase spheres and giving low softening point pitches [5, 31]. Therefore, pitch molecules should contain a certain number of naphthenic groups and short alkyl side chains to get a good-quality mesophase pitch having high softening point and also exhibit better optical texture of mesophase. Also, the hydrogen aromaticity index (H_{ar}/H_{al}) of prepared pitches follows the trend CLO-Cr-3>CLO-Cu-3>CLO-0-0 which also suggest that Cr and Cu enhances the polymerization/condensation reactions during the thermal soaking occur at the expense of aliphatic hydrogen. Like ¹H NMR spectra, ¹³C NMR spectroscopy also supports the above findings of pitches whose integration data are listed in Table 3. The effect of Cr and Cu catalysts on hydrogen (H_{ar}/H_{al}) and carbon aromaticity (C_{ar}/C_{sat}) is similar to that observed for aromaticity (C/H ratio Table 2, I_{ar} by FT-IR in Fig. 4).

XRD analysis of mesophase pitches

XRD of CLO-Cr-3 and CLO-Cu-3 pitches prepared from CLO using transition metal catalysts is shown in Fig. 6. As seen in the figure, the diffractogram of CLO-Cr-3 and CLO-Cu-3 shows two broad peaks at approximately 25.5° and 45°, which corresponds to the graphite-like carbon material. First peak at 25.5° is a strong peak which indicates that pitches primarily had (002) crystal planes corresponding to carbon structures due to the stacking of aromatic layers and at 45°, weak broad peak appears which corresponds to pitches that



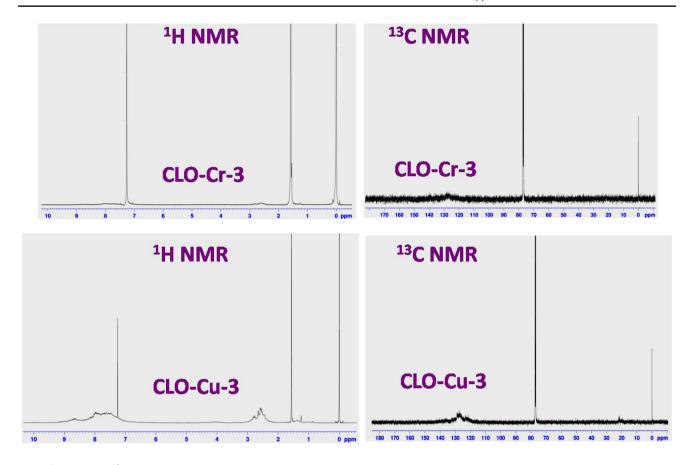


Fig. 5 ¹H NMR and ¹³C NMR spectra of synthesized petroleum pitches

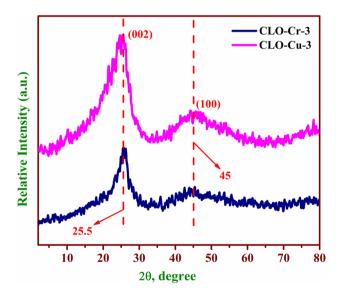


Fig. 6 X-ray diffractograms of synthesized petroleum pitches

partially had (100) crystal planes. These two peaks (002) and (100) are assigned to amorphous carbon. Other parameters such as crystallite thickness (L_c), interlayer spacing (d_{002}), number of aromatic sheet stacked in cluster (N) and average

Table 4 X-ray diffraction parameters of pitches

Sample	CLO-0-0 [9]	CLO-Cr-3	CLO-Cu-3
$L_{c} (\mathring{A})$ $d_{002} (\mathring{A})$	9.85	17.97	15.51
$d_{002}(\mathring{\mathrm{A}})$	3.636	3.443	3.523
N^a	3	6	5
n^{b}	3	12	8

 $^{{}^{}a}N = L_{c}/d_{002} + 1$ where N is ordered stacking number

number of carbon atom per lamellae (n) are also calculated from these diffractograms listed in Table 4. The crystallite thickness (L_c) , number of aromatic sheet stacked in cluster (N) and average number of carbon atom per lamellae (n) are found to be varying from 15.51 to 17.97, 5 to 6 and 8 to 12, respectively, for pitch samples. Table 4 shows that L_c , N and n values of CLO-Cr-3 and CLO-Cu-3 pitches are increased together with a decrease in their interlayer distance (d_{002}) as compared to CLO-0-0 pitch whose parameters are reported in our previous paper [9]. The increased value of L_c , N and n indicates that transition metal salts (Cr and Cu) promote the polymerization and condensation reactions in paraffinic CLO which result in the formation of parallely



^bAverage number of carbon atom per lamellae (n) where $n = 0.32N^2$

stacked planar aromatic molecules, i.e., mesophase molecules. Furthermore, in XRD, no extra peaks of Cr and Cu were observed in pitches which show that these transition metal salts do not attach with pitch molecule. These results are also consistent with SEM–EDX spectra results. Further, L_c and N trends from the XRD analysis correspond to the C/H ratios (Table 2) and $I_{\rm ar}$ (Fig. 4) related to the aromatic contents.

TGA analysis of mesophase pitches

The thermal decomposition properties of synthesized petroleum pitches were probed over the temperature range of 40–900 °C which is shown in Fig. 7. Figure 7 explicitly shows that CLO-Cu-3 and CLO-Cr-3 petroleum pitches exhibited higher thermal stability than CLO-0-0 petroleum pitch. The higher thermal stability of CLO-Cu-3 and CLO-Cr-3 petroleum pitches is due to the presence of aromatic rings in their complex polynuclear aromatic structure. It was noted that all petroleum pitches thermally decomposed in the range of 210-550 °C. Temperature of initial weight loss (T_i) , temperature of final weight loss (T_f) , and temperature of maximum rate of weight loss (T_{max}) calculated from TG/DTG curves are shown in Fig. 7 and Table 5. The initial weight loss can be ascribed to the distillation of low-molecular weight hydrocarbons, while the final weight loss may be due to the removable of light hydrocarbon molecules from the pitch samples which are cracked during pyrolysis. DTG curves show that temperature of maximum rate of weight loss of both CLO-Cu-3 and CLO-Cr-3 pitches occurred between 300 and 350 °C approximately which indicates that complex polycyclic aromatic hydrocarbons are present in it. Table 5 shows

Table 5 TG and DTG parameters of pitch samples

Sample	CLO-0-0 [9]	CLO-Cr-3	CLO-Cu-3
TG/DTG (°C	C)	,	
$T_{\rm i}^{ m a}$	185	199	215
$T_{ m f}^{ m b}$	480	530	538
$T_{\rm max}^{\rm c}$	347	308	342
\mathbf{M}^{d}	70.02	44.39	58.10
CY^e	29.98	55.61	41.90

^aTemperature of initial weight loss (°C)

that in the temperature range of 40-900 °C, CLO-Cr-3 and CLO-Cu-3 pitches lost 44.39 and 58.10 wt % of their original mass. The weight loss of both the pitch samples was ceased at approximately 550 °C. The flat pattern of the TG curve over 550 °C corresponds to coke formation [3]. In addition, we can also calculate carbonization yield of pitch samples from TGA curve (Fig. 7) which is listed in Table 5. Carbonization yield obtained from TGA curves at 900 °C showed that CLO-Cr-3 and CLO-Cu-3 pitches have more carbon residue yield as compared to CLO-0-0 pitch which suggested that catalyst promotes the polymerization and condensation reactions which result in the formation of more complex polycyclic aromatic hydrocarbons. Furthermore, this finding indicates that copper and chromium catalysts facilitate more polymerization and condensation reaction during thermal soaking of pitch formation.

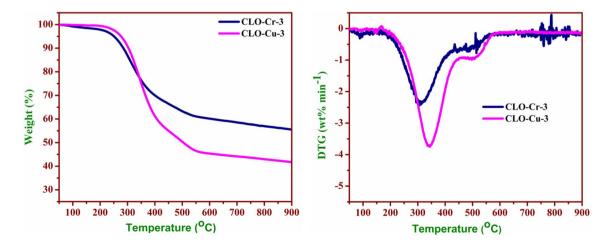


Fig. 7 Thermogravimetric (left) and derivative thermogravimetric (right) curve of synthesized petroleum pitches



^bTemperature of final weight loss (°C)

^cTemperature of maximum weight loss rate (°C)

dMass lose (wt %)

^eCarbonization yield at 900 °C (wt %) (carbonization yield = 100 – weight loss of mesophase pitch)

Conclusions

The focus of this work was to synthesize petroleum mesophase pitches from paraffinic clarified oil by transition metal catalysts (i.e., Cr and Cu) as precursor material for advanced carbon products and also study the effect of these catalysts on physico-chemical properties. Generally, paraffinic hydrocarbons are undesirable for making mesophase pitches but their attachments on aromatic molecules are necessary because they generate free radicals for polymerization reaction. Optical microscopic results show that Cu and Cr enhance the growth of mesophase spheres and also increase the mesophase contents. Therefore, Cu and Cr promote the parallely stacked aromatic mesophase formation in pitches through a series of reactions such as cracking, polymerization, condensation, etc. The higher value of crystallite thickness of CLO-Cu-3 and CLO-Cr-3 as compared to CLO-0-0 also indicates that there is a high degree of polymerization. NMR, FT-IR and CHNS analyses also support the higher degree of polymerization for CLO-Cu-3 and CLO-Cr-3 mesophase pitches. In addition, SEM images clearly indicated that catalysts increase the size of pitch flakes but they are not attached on the surface of pitch molecules. Therefore, the present study shows that Cu and Cr catalysts have higher catalytic activity for mesophase formation growth. It was further observed that Cu and Cr catalysts are also helpful for increasing physico-chemical properties of mesophase pitches.

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